

Preparation and characterization of molybdenum disulphide catalysts

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Molybdenum disulphide has been prepared by atmospheric-pressure hydrogen reduction of molybdenum trisulphide in the temperature range 400–750 °C for 4 h and characterized. Chemical analysis of the product confirmed the S to Mo ratio 2.00 as desired for MoS₂, consistent with its thermogravimetric analysis data in an air atmosphere. MoS₂ prepared under these reducing conditions possessed a hexagonal structure with n-type diamagnetic semiconducting behaviour and a lower surface area. The catalytic activity of the MoS₂ was studied for liquid-phase hydrogenation of nitrobenzene. X-ray studies on MoS₃ when reduced at 750 °C for 48 h indicated that MoS₂ so formed is unstable, resulting in the formation of its over-reduced products Mo₂S₃ and Mo.

1. Introduction

Layered transition metal dichalcogenides of groups IVB, VB and VIB constitute structurally and chemically a well-defined family of compounds whose physical and chemical properties have stimulated a considerable amount of interest during the past few years [1–3]. The most striking feature of these compounds is that they crystallize in a quasi-two-dimensional layer type of structure which imparts substantial anisotropy to most of their physical properties. In addition, this layer structure facilitates the process of intercalation to form stoichiometric and non-stoichiometric compounds with metal atoms, organic and inorganic molecules [4]. These layered transition metal dichalcogenides and their intercalation compounds are useful materials in the field of catalysis [5], high temperature–high pressure lubricants [3] and in solar energy conversion [6], etc.

Molybdenum disulphide, MoS₂, is representative of these materials and is most promising for modern uses [7–13]. It crystallizes in a layered structure. There exists a trigonal prismatic coordination between molybdenum and sulphur atoms within each layer and bonding is primarily covalent. The structure is characterized by the presence of Mo⁴⁺ and S²⁻ sheets where each Mo⁴⁺ sheet is sandwiched between two S²⁻ sheets. The sandwiched sheets are held together by weak van-der Waals forces. Molybdenum disulphide is also used as a catalyst for hydrogenation in those cases where the raw materials are not pure and contain catalytic poisons, particularly sulphur compounds [5, 14–17]. However, not much information is available about kinetic and mechanistic features of the hydrogenation of nitrobenzene over MoS₂ and the change if any in the catalyst system.

The present paper deals with the preparation of MoS₂ by atmospheric pressure reduction of MoS₃ and characterization by various physico-chemical methods. Attempts have also been made to assess the

suitability of this material as a catalyst in hydroxylation reactions like the hydrogenation of nitrobenzene to aniline. Further, the MoS₂ catalyst used has also been characterized and the results have been utilized to explain the catalytic activity of MoS₂ for this reaction.

2. Experimental procedure

2.1. Sample preparation

The base material MoS₃ was prepared by solid-state reaction of MoO₃ and thiourea at 130 °C [18]. The reduction of 5 g of MoS₃ was carried out in an electrically heated furnace by passing a stream of hydrogen with a flow rate of 60 cm³ min⁻¹. Different samples of MoS₂ were prepared at 400, 500, 600 and 750 °C for 4 h and at 750 °C for 48 h. The furnace was then switched off but the flow of hydrogen was continued through the system until it cooled down to room temperature. Finally, the sample was taken out.

2.2. Characterization

MoS₂ was analysed by the conventional chemical analytical method [19]. Molybdenum was estimated by the oxime method and sulphur as BaSO₄.

X-ray diffractograms of the samples were obtained with a Philips 1720 diffractometer using CuK_α radiation ($\lambda = 0.15418$ nm). Each pattern was recorded in the range $5^\circ < 2\theta < 60^\circ$ with a scan rate of $1^\circ/2\theta$ min⁻¹ and a chart speed of 0.1° mm⁻¹. The particle size for each specimen was calculated using the Scherrer formula

$$t = k\lambda/\beta \cos \theta_0$$

where t is the particle size as measured perpendicular to the reflecting plane, k is the Scherrer constant (taken as unity, assuming the particles to be spherical in shape), λ is the wavelength of the X-ray radiation, β

is the half-intensity width measured in radians and θ_0 is the Bragg angle.

Room-temperature magnetic susceptibility was measured by using the Guoy method in a field strength of about 30.06 G. The balance was initially calibrated using $\text{Hg}[\text{Co}(\text{SCN})_4]$ as a standard. The type of conductivity was determined by simple thermoelectric power experiments. The conductivity measurements were made using a two-probe technique on compressed pellets in the temperature range 25–350 °C. Thermogravimetric analyses were performed in an air atmosphere with a programmed heating rate of 10 °C min^{-1} up to 1000 °C. The surface area for MoS_2 samples was measured by the BET method.

The catalytic activity of MoS_2 in the hydrogenation of nitrobenzene was tested in a high-pressure autoclave, details of which are given elsewhere [20]. The products were analysed by gas-liquid chromatography using an SE-30 column.

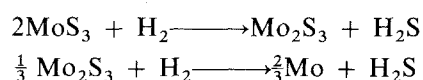
3. Results and Discussion

3.1. Characterization

The chemical analysis of the product confirmed the sulphur to molybdenum ratio of 2.00 for MoS_2 .

The X-ray diffractograms of molybdenum disulphide prepared by reducing MoS_3 at 400, 500, 600 and 750 °C for 4 h each are shown in Fig. 1a–e respectively. The absence of any peak for MoS_3 confirmed its amorphous character. However, the d -values for its reduced product were found to be in good agreement with the data reported for hexagonal MoS_2 [21]. The diffractograms showed a strong orientation of the 002 peak along the c axis. It is also evident from Fig. 1 that the increase of intensity of the 002 reflection with increasing reduction temperature was more pronounced in comparison to other 00 l reflections. The intensity of other reflections such as 10 l , 11 l also improved but to a lesser extent. The lattice parameters were also calculated for MoS_2 (Table I) and were in agreement with the values reported by Al-Hilli and Leonard [22]. The X-ray diffractograms of MoS_3 when reduced at 750 °C for 48 h showed that the 002 line of maximum intensity in MoS_2 had disappeared and a few new sharp lines were present (Fig. 1f). These closely corresponded to Mo_2S_3 and metallic molybdenum. In addition, some lines of weak intensity due to unreduced MoS_2 were also observed.

Our results show that MoS_3 is reduced to metallic molybdenum via the following steps:



Calculation of the particle size for MoS_2 showed that there is slight anisotropy along the a and c axes, which diminishes with increasing reduction temperature (Table II).

Room-temperature magnetic susceptibility measurements and thermoelectric power experiments indicated that MoS_2 prepared by different methods is diamagnetic and possessed n-type conductivity (Tab-

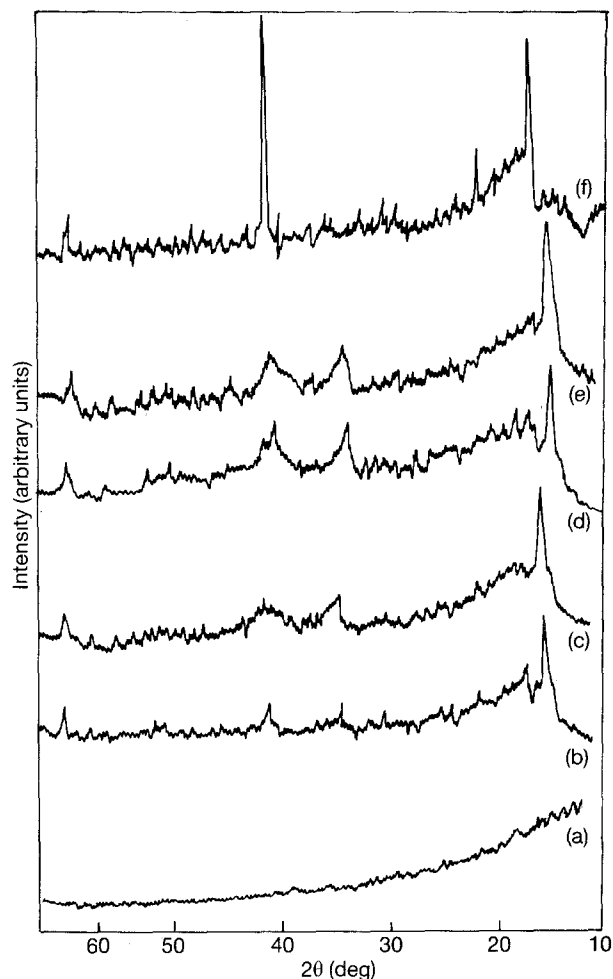


Figure 1 X-ray diffractograms for (a) MoS_3 and when reduced for 4 h at (b) 400 °C, (c) 500 °C, (d) 600 °C and (e) 750 °C, and at (f) 750 °C for 48 h.

TABLE I Unit cell dimensions of MoS_2

Reduction temperature (°C)	a (nm)	c (nm)	c/a	$V(\text{nm})^3$
400	0.3162	1.2271	3.890	0.1065
500	0.3162	1.2273	3.881	0.1062
600	0.3160	1.2274	3.884	0.1061
750	0.3163	1.2276	3.880	0.1063

TABLE II Particle size distribution for MoS_2

hkl	Partical size (nm)			
	400 °C	500 °C	600 °C	750 °C
100	11.51	12.23	12.94	13.42
103	13.72	12.93	13.46	14.80
110	13.53	14.10	14.60	15.63
008	17.00	16.23	17.04	17.94

le III). Conductivity (σ) measurements on MoS_2 in the temperature range 303–573 K confirmed its semiconducting behaviour (Fig. 2). From the plot of $\ln\sigma$ versus $10^3/T$, the value of activation energy, E_a , was calculated using the expression

$$\sigma = \sigma_0 \exp(-E_a/kT)$$

TABLE III Room-temperature magnetic susceptibility (χ), Seebeck coefficient (S), conductivity (σ) and activation energy (E_a) data for MoS₂

Reduction temperature (°C)	$(\chi_{300\text{K}})$ (10^{-6} e.m.u.)	$S_{300\text{K}}^{\circ}$ ($\mu\text{V } ^{\circ}\text{C}^{-1}$)	$\sigma_{300\text{K}}$ ($\Omega^{-1}\text{ cm}^{-1}$)	E_a (eV)	Surface area ($\text{m}^2\text{ g}^{-1}$)
400	-0.158	-410	2.14×10^{-5}	0.22	2.50
500	-0.065	-390	1.88×10^{-5}	0.17	2.89
600	-0.720	-255	1.67×10^{-5}	0.18	3.30
750	-0.503	-274	4.1×10^{-6}	0.27	3.50

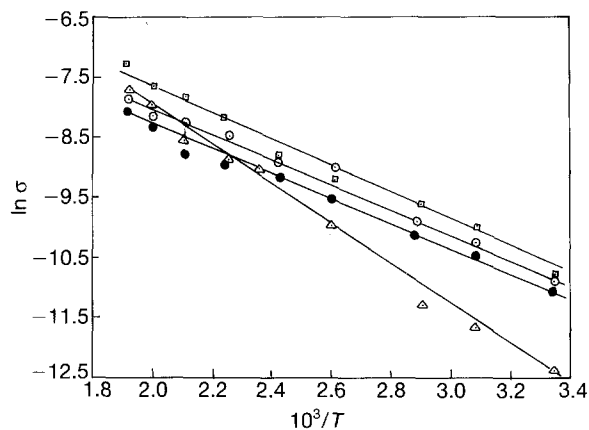


Figure 2 Temperature dependence of electrical conductivity (σ) for MoS₂ prepared at different reduction temperatures: (\square) 400°C, (\circ) 500°C, (\bullet) 600°C and (\triangle) 750°C,

The smaller values of E_a (Table III) probably refer to extrinsic (impurity) conduction process. However, the changes in the values of σ_{RT} and E_a may be a result of changes in the time and temperature of MoS₂ preparation, or due to small changes in stoichiometry or imperfections which act as scattering centres.

3.2.1. Used catalysts

Used catalysts were also characterized by chemical analysis, X-ray diffractometry and thermal analysis to establish the nature of the surface which has suffered deactivation.

Chemical analysis and X-ray diffraction pattern did not reveal any significant change in composition or any phase change of the used catalyst. Since MoS₂ catalyst is characterized by a very low surface area ($2.86\text{ m}^2\text{ g}^{-1}$), it appears that only a small amount of aniline accumulated on the surface will be sufficient to stop further hydrogenation of nitrobenzene. Such a small amount of aniline may not be able to effect any conceivable change either in the composition or any consequent changes in the unit cell dimensions. Intercalation of aniline in MoS₂, which is quite possible, is not likely to be detected by X-ray diffractometry, since no change in X-ray parameters has been observed with the intercalation compounds of MoS₂ with NH₃ [23]. These intercalated compounds are highly susceptible towards decomposition when exposed to air or moisture.

Differential thermal analysis of the fresh and used catalysts provided substantial proof in favour of accumulated aniline on the MoS₂ surface (Fig. 3). It is evident from the thermograms that the thermal beha-

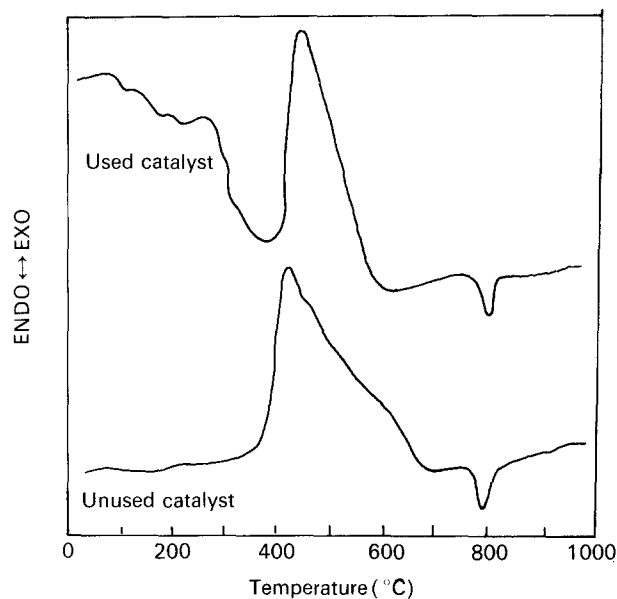


Figure 3 Thermograms of pure and used MoS₂ catalyst.

viour of MoS₂ in air is significantly altered after being used in the reaction, although a common trend is retained. When heated in air, freshly prepared MoS₂ exhibited two distinct peaks, one highly exothermic, starting at 340°C and ending at 665°C with a peak at 425°C, and another endothermic one starting at 750°C and ending at 805°C with a peak at 790°C. The first peak is due to the oxidation of MoS₂ to MoO₃ and the second one to melting of MoO₃. With used MoS₂, the corresponding temperatures for the first thermal change are considerably shifted, while those for the second phase remain essentially the same. Additional differences that could be observed in the thermogram of the used MoS₂ catalyst are a series of several endothermic peaks occurring at 180, 210, 270, 290 and 405°C just before the onset of oxidative decomposition of MoS₂. Endotherms at 180 and 210°C are easily identifiable as those due to imbibed aniline and nitrobenzene, respectively. Other endotherms beyond 210°C are likely to be due to desorption of some of the products originating from oxidative decomposition of aniline and nitrobenzene or from their interaction with MoS₂ itself at higher temperature.

The two distinct phases as observed in the time-conversion plots under different experimental conditions of temperature and pressure are now easily understood (Figs 4 and 5). The first phase, in which conversion rises steadily to a maximum value, corresponds to the slow accumulation of product aniline on

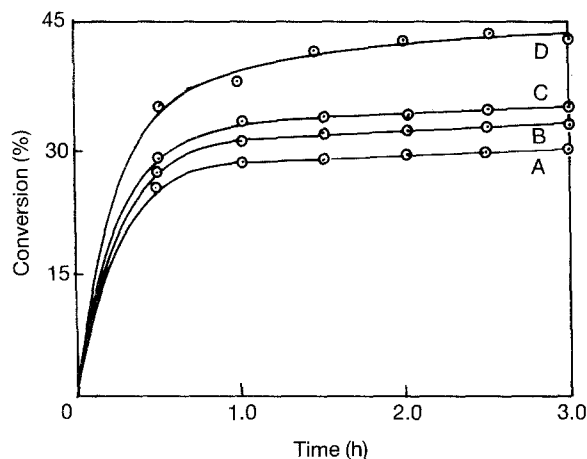


Figure 4 Time-conversion plots for conversion of nitrobenzene in the presence of MoS_2 catalyst at (A) 110°C , (B) 135°C , (C) 150°C and (D) 180°C ; catalyst amount 20 g l^{-1} , H_2 pressure $3.44 \times 10^6\text{ N m}^{-2}$.

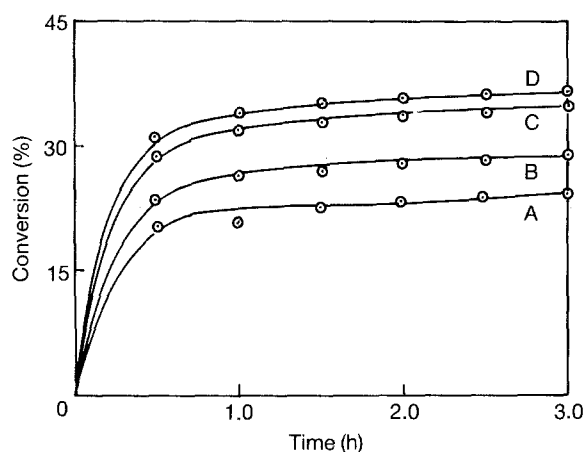


Figure 5 Time-conversion plots for conversion of nitrobenzene in the presence of MoS_2 catalyst at H_2 pressure (A) 2.06×10^6 , (B) 2.95×10^6 , (C) 3.44×10^6 and (D) $4.13 \times 10^6\text{ N m}^{-2}$; catalyst amount 20 g l^{-1} , temperature 150°C .

the MoS_2 surface up to a point of saturation. Beyond this, the second phase starts in which the reaction is virtually totally arrested and conversion remains almost constant, even up to 3 h.

3.2. Surface interaction between catalyst and product

Some secondary interactions between the catalyst and the product aniline appear to be theoretically very much favoured. Aniline being a proven base and MoS_2 an n-type semiconductor, a strong cumulative adsorption is predictable on the basis of Hauffe's electrical double layer theory [24]. Also, in view of the acidic character of MoS_2 , a strong interaction between aniline and the catalyst is indicated. Furthermore, Mo(IV) is known to form stable amine complexes [25] which may effectively alter the surface characteristics of MoS_2 .

4. Summary and conclusion

Molybdenum disulphide has been prepared by atmo-

spheric pressure reduction of MoS_3 in the temperature range $400\text{--}750^\circ\text{C}$ for 4 h. It was found to be an n-type diamagnetic semiconductor with a surface area varying in the region of $2.35\text{ m}^2\text{ g}^{-1}$. MoS_2 has also been used as a catalyst in liquid-phase hydrogenation of nitrobenzene and then characterized. The reaction was found to be partially complete with aniline as the only product. Possibly the surface accumulation of aniline on the catalyst surface as a strongly adsorbed species or the formation of an intercalated compound makes the MoS_2 surface completely inactive against further hydrogenation. With all these possibilities taken together, it appears that the surface of the catalyst is progressively covered with aniline as the reaction progresses, debarring the nitrobenzene from further adsorption on the catalyst surface. Thus the observed second phase in the time-conversion plots (Figs 4 and 5) may be explained in terms of a situation where the surface of the catalyst is virtually unavailable to nitrobenzene for further hydrogenation.

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